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## First example of organocatalysis by cathodic Nheterocyclic carbene generation and accumulation using a divided electrochemical flow cell.

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### Abstract

It is well known that the electrochemical reduction of 1-butyl-3-methylimidazolium tetrafluoroborate (BMImBF<sub>4</sub>) yields the corresponding N-heterocyclic carbene (NHC). This carbene is quite unstable and its main use is as an organocatalyst in umpolung

reactions of aldehydes. Due to its instability, NHC quantification can be indirectly carried out through its transformation into the corresponding thione, by reaction with elemental sulfur. The cathodic generation is carried out in a divided cell, as NHCs readily oxidise at the anode. The need for high amounts of supporting electrolyte is one of the major drawbacks of batch electrochemistry, which can be addressed by using flow electrolysis cells with small interelectrode gaps. In flow cells the distance between the two electrodes can decrease to such an extent that sometimes no supporting electrolyte is needed, offering additional benefits such as simplification of product isolation. Moreover, flow electrochemistry can provide higher rates of conversion compared to batch. Only one paper in the literature reports NHC generation by cathodic reduction of an imidazolium salt, in a undivided cell, in which the NHC oxidation problem is overcome by the use of a sacrificial anode (Cu), which releases Cu<sup>+</sup> ions to form NHC-Cu complexes. In this paper we present the first electrochemical generation of NHC carried in a divided flow cell with NHC accumulation and subsequent use as organocatalyst. We demonstrated not only the NHC accumulation (indirectly by reaction with elemental sulfur), but also the possibility to use this NHC in two classical umpolung reactions of cinnamaldehyde: its cyclodimerization and its oxidative esterification.

### Keywords

Flow Electrochemistry; N-heterocyclic carbene; Breslow intermediate; oxidative esterification; cathodic reduction

## Introduction

lonic liquids (ILs) are well known salts, at present used in a wide variety of chemical fields. The first definition of ionic liquids was given by Paul Walden in 1914: "*they are materials composed of cations and anions, that melt around 100* °C *or below as an arbitrary temperature limit*" [1]. At present, ILs are considered as a class of salts resulting from the association of large organic cations (tetraalkylammonium, tetraalkylphosphonium, 1,3-dialkylimidazolium, N-alkyl-pyridinium, etc.) with weakly coordinating anions (<sup>-</sup>BF<sub>4</sub>, <sup>-</sup>PF<sub>6</sub>, <sup>-</sup>N(CF<sub>3</sub>SO<sub>2</sub>)<sub>2</sub>, etc.) [2, 3].

The physico-chemical properties of RTILs (room temperature ionic liquids) have been reported by many authors, which include negligible vapour pressure, low flammability, broad solubility range, high thermal and chemical stabilities, catalytic properties (they can act both as solvents and as catalysts), large electrochemical window, high electrical conductivity, possible recycling, ability to increase reactivity as well as the selectivity of some processes and facile product separation [4, 5]. Among ILs, imidazolium derivatives are one of the most studied, in part due to their ease of synthesis, low cost and diverse applications from solvents and reagents in synthesis, to supporting electrolytes in electrochemistry [6].

The imidazolium cation can be modified by the presence of a base or by a single electron cathodic reduction of the C–H between nitrogen atoms of imidazolium ring (Scheme 1), inducing the formation of a N-heterocyclic carbene (NHC) [7, 8]. In recent years, NHCs have achieved great success: they have been frequently used as ligands in organometallic catalysts [9] and as versatile organocatalysts [10] in a very wide range of organic reactions such as classical benzoin condensation, transesterification, acylation, Knoevenagel reaction, Claisen condensation etc.



Scheme 1: Electrochemical generation of NHC.

Electrochemical generation of carbenes from ILs avoids the use of strong bases and the formation of by-products (dimers of carbene and nitrogen dealkylation products),

where the IL acts as NHC precursor, solvent, and supporting electrolyte, needing no additional chemicals in the electrolytic cell [11]. An added attraction of this approach is that unstable NHCs are generated in situ, where they may be used as basic or nucleophilic species. Due to the difficulty isolating highly reactive NHCs, the concentration of the obtained NHC solution can be determined indirectly by addition of elemental sulfur after the electrolysis, which realizes quantitative conversion to the corresponding thione (Scheme 2) [12].



**Scheme 2:** Transformation of electrochemically generated NHC into the corresponding thione by its reaction with elemental sulfur.

NHCs are used as organocatalysts in many reactions of aldehydes (mainly aromatic) [13, 14]. In fact, reaction of NHCs with aldehydes can lead to the formation of the "Breslow intermediate" [15], in which the reactive character of carbonyl carbon atom is reversed (umpolung) from electrophilic to nucleophilic (Scheme 3).



**Scheme 3:** Umpolung of the aldehyde carbonyl carbon atom. Formation of the Breslow intermediate using NHCs.

This approach can be exploited in many organic reactions, such as: the benzoin condensation [16, 17], esterification and amidation of benzaldehydes and cinnamaldehydes [18, 19], synthesis of  $\gamma$ -butyrolactones [20], synthesis of 1,3-diketones [21], etc.

Electrosynthesis is considered as a more sustainable approach to perform chemical reactions, and an interesting alternative to conventional synthetic methods both in laboratory and industry processes. In fact, the electron may be considered to be a

clean reagent, which replaces toxic chemical redox reagents and dangerous procedures [22-25]. At present, electrosynthesis in batch is more widely used and reported in literature, but some disadvantages can be encountered: the need for high concentrations of supporting electrolyte, poor performance for synthesis such as slow rates of conversion, low selectivity and reproducibility [26]. As a matter of fact, these problems can be addressed by using flow electrochemistry, usually achieving higher rates of conversion of reagents to products [27]. Moreover, using electrochemical flow cells it is possible to have a very small gap between the electrodes and so that lower concentrations of supporting electrolytes are needed to provide sufficient conductivity [28]. Applications of Flow Electrochemistry reported in the literature are mainly devoted to anodic oxidations, carried out in undivided cells, in which the counter electrode reaction at the cathode is usually H<sub>2</sub> evolution [29]. The use of divided cells is less common in organic electrosynthesis, mainly due to complications inherent with membranes. Useful cathodic processes are less exploited in organic electrochemistry. In the context of NHC organocatalysis in Flow Electrochemistry, NHC instability (and anodic electroactivity) prevented its cathodic generation and subsequent use as catalyst or reagent. Instead, the NHC was generated by chemical deprotonation using a strong base (DBU) and then applied in anodic esterification [30-32], and amidation of aromatic aldehydes [33]. Flow Electrochemistry was applied to oxidise the Breslow intermediate to the corresponding electrophilic acylthiazolium intermediate, which then functioned as an acyl-transfer reagent, reacting with alcohols or amines. To the best of our knowledge, only one research group reported the cathodic reduction of an imidazolium cation to NHC, in an undivided cell under flow conditions, coupled with the anodic generation of Cu(I) from a sacrificial anode to yield the corresponding N-heterocyclic carbene complex [34, 35]. In this case, irreversible capture of the NHC by the metallic cation prevented NHC oxidation/degradation.

In this paper we describe the cathodic generation and accumulation of NHC in a divided flow cell (for the first time) and its subsequent use as organocatalyst in the self-annulation of cinnamaldhyde and in the esterification of cinnamaldehyde.

## **Results and Discussion**

# Cathodic NHC generation and accumulation using a divided flow electrochemical cell. Quantification of NHC in IL solution.

The flow cell used in this work was previously described [36] and is based on two electrode plates separated by a spacer/gasket fabricated from an PTFE sheet with its center cut away to form the electrolyte flow chamber (Figure 1). The requirement for a divided cell (a more complicated device than the undivided configuration) arises from the need to protect electrogenerated NHC from its anodic oxidation in the absence of a consumable anode.





To ensure good sealing of the electrolysis cell, the sandwich-type arrangement of cell components was compressed between two end plates using a series of bolts. This design incorporated a solution inlet and a solution outlet for the chamber to allow uniform flow over the surface of the electrodes. In the present work, where a divided cell configuration was required, a proton-permeable membrane (Nafion® 438) was inserted to separate the cathode and anode chambers, and a spacer was now used on each compartment [36].

The initial goal of this work was to demonstrate the possibility to achieve NHC formation starting from 1-butyl-3-methylimidazolium tetrafluoroborate (BMImBF<sub>4</sub>), by cathodic reduction in a divided cell using flow electrochemistry technique, and to compare the results with the corresponding batch process. Once established, the flow electrochemistry NHC synthesis would be combined with applications as an organocatalyst in some organic transformations of cinnamaldehyde.

Firstly, the conditions for electrogeneration of the carbene in flow were optimized, quantifying the amount of NHC by means of its reaction with elemental sulfur. All the experiments were carried out using a 0.1 M solution of BMImBF<sub>4</sub> in acetonitrile as catholyte in a divided cell using Nafion® 438 membrane, under N<sub>2</sub> atmosphere, at room temperature, under galvanostatic conditions (I = 134 mA) with continuous flow rate of 36 mL/min, studying the effect of cathode material, anode solution and number of Faradays per mole of IL supplied (Table 1). At the end of the electrolysis, excess elemental sulfur was added to the catholyte and the mixture was left under ultrasound irradiation for 30 minutes. The solvent was removed under reduced pressure and the residue was purified by column chromatography on silica gel.

The first experiment (Table 1, entry 1) was carried out using stainless steel as cathode and a carbon-filled polyvinylidene fluoride (C/PVDF) plate as anode. BMImBF<sub>4</sub>/MeCN 0.1 M in acetonitrile was the catholyte, while the anolyte was a solution of tetraethylammonium tetrafluoroborate (Et<sub>4</sub>NBF<sub>4</sub>) in acetonitrile; after only 12 minutes of electrolysis the current flow stopped. Moreover, a consumption of anode was observed (Figure 2). It is possible that, in the absence of a suitable counter electrode process, the tetrafluoroborate anion was itself oxidized [7] leading to erosion of the anode with the formation of fluorocarbons.



**Figure 2:** C/PVDF anode before (A) and after (B) the first experiment (Table 1, entry 1)

In order to avoid anode consumption/passivation, an alternative to oxidation of BF<sub>4</sub><sup>-</sup> was required as the counter electrode reaction, and 10% of methanol was added to the anolyte solution. In this case (Table 1, entry 2) 13% of thione was obtained and the electrode did not show any signs of consumption. The same yield (13%) was obtained using nickel as cathode material (entry 4). However, using a silver electrode the corresponding thione was not observed (entry 3). In view of the acidic character of the perfluorosulfonic acid Nafion® membrane, and possible NHC protonation to return the imidazolium cation, the Nafion® membrane was pretreated with an alkaline solution for 24 hours in order to try to increase the thione yield. Using stainless steel as cathode and a lower amount of methanol at the anode the quantity of thione increased to 21% (Table 1, entry 5). Under the same conditions, but using dry acetonitrile, the best yield was obtained (32%, entry 6); in this case a small amount of imidazolone 1b (<5%) was observed from the NMR spectrum, probably due to the reaction with adventitious oxygen. It should be underlined that in these electrolyses BMImBF<sub>4</sub> acts as both electroactive species and supporting electrolyte, and although the cathodic reduction of the imidazolium cation is a monoelectronic process, in similar process carried out in batch the current yield usually does not exceed 50%, thus rendering necessary an excess of current [37]. The yields reported in Table 1 (entries 2 to 6) are obtained using a stoichiometric amount of electricity (1 electron per imidazolium cation). Therefore, the 32% chemical yield (with respect to starting IL) is comparatively favourable with the batch process.

	M	e Me		Ме		Ме
		$\frac{+e^{-}}{-0.5 H_2}  [\bigwedge_{N}^{N} : \frac{+e^{-}}{-e^{-}}]$	S <sub>8</sub> ►		6 + ( <sup>N</sup>	
	Bı	u Bu		Bu		Bu
	BMIr	n <sup>⁺</sup> NHC		1a		1b
Entry	Cathode material	Anolyte	Q (F)	Time (min)	Yield 1a <sup>c</sup>	Notes
1	SS₫	MeCN/Et₄NBF₄ 0.05 M, 25 mL	0.5	12	<5%	anode erosion
2	SS₫	MeCN:MeOH (9:1) /Et₄NBF₄ 0.05 M, 25 mL	1.0	24	13%	-
3	Ag	MeCN:MeOH (9:1) /Et₄NBF₄ 0.05 M, 25 mL	1.0	24	-	-
4	Ni	MeCN:MeOH (9:1) /Et <sub>4</sub> NBF <sub>4</sub> 0.05 M, 25 mL	1.0	24	13%	-
5	SS₫	MeCN:MeOH (9.5:0.5) /Et₄NBF₄ 0.1 M, 20 mL	1.0	24	21%	Nafion® alkaline pretreatment
6	SS₫	Dry MeCN:MeOH (9.5:0.5) /Et <sub>4</sub> NBF <sub>4</sub> 0.1 M, 20 mL	1.0	24	32% ( <b>1b</b> <5%)	Nafion® alkaline pretreatment

**Table 1**: Electrochemical reduction of BMImBF<sub>4</sub>,<sup>a</sup> followed by the addition of elemental sulfur<sup>b</sup>. Flow cell, in recycling mode.

<sup>a</sup>Divided cell, carbon-filled polyvinylidene fluoride (C/PVDF) anode material, Nafion® 438 membrane separator, room temperature, N<sub>2</sub> atmosphere, galvanostatic conditions (134 mA), catholyte: BMImBF<sub>4</sub>/MeCN 0.1 M, 20 mL (2 mmol BIMImBF<sub>4</sub>); <sup>b</sup>Excess S<sub>8</sub> (2 mmol) added at the end of the electrolysis to the catholyte. Then energy was supplied to the catholyte (ultrasound irradiation, 35 W) for 30 minutes; <sup>c</sup>Isolated yields, based on starting IL (BIMImBF<sub>4</sub>); <sup>d</sup>Stainless steel.

## Electrogenerated NHC organocatalysis. Dimerization of *trans*cinnamaldehyde: synthesis of 4-phenyl-5-styryldihydrofuran-2(3*H*)-

#### one

Having demonstrated that NHC could be generated and accumulated in a continuous flow electrochemical process, the flow methodology was applied to the self-annulation of cinnamaldheyde, a classical NHC-catalysed reaction (Scheme 4).



Scheme 4. Electrogenerated NHC catalysed self-annulation of cinnamaldheyde.

All the experiments were carried out using a solution 0.1 M of BMImBF<sub>4</sub> in acetonitrile (20 mL) as catholyte, stainless steel as cathode, C/PVDF as anode, in a divided cell, under N<sub>2</sub> atmosphere, at room temperature, under galvanostatic conditions (I = 134 mA) with flow rate of 36 mL/min, changing anode solution and number of Faradays per mole supplied (Table 2). Following the experimental results previously obtained, the Nafion® membrane was always pretreated with an alkaline solution. At the end of the electrolysis, 1 mmol of cinnamaldehyde was added to the catholyte and the mixture was left under stirring for two hours at room temperature. Workup and

column chromatography yielded a diastereomeric mixture of γ-butyrolactones **2a** and **2b**.

$BMIm^{+} \xrightarrow{+e^{-}}_{-0.5 \text{ H}_{2}} \text{ NHC}$ $NHC + Ph \xrightarrow{\bigcirc}_{H} H \xrightarrow{\bigcirc}_{Ph} + Ph \xrightarrow{\bigcirc}_{Ph} Ph$					
		(	<u>+</u> )- <b>2</b> a	( <u>+</u> )- <b>2b</b>	
Entry	Anolyte	Q (F) <sup>b</sup>	Time (min)	Yie 2a	eld <sup>c</sup> 2b
1	MeCN:MeOH (95:5)/Et4NBF4 (0.1M), 20 mL	0.25	6	15%	8%
2	MeCN:MeOH (95:5)/Et4NBF4 (0.1M), 20 mL	0.50	12	43%	24%
3	MeCN:MeOH (95:5)/Et4NBF4 (0.1M), 20 mL	1.00	24	53%	26%
4	MeCN:MeOH (98:2)/Et <sub>4</sub> NBF <sub>4</sub> (0.1M), 20 mL	0.50	12	42%	32%
5	MeCN:DMSO(95:5)/Et <sub>4</sub> NBF <sub>4</sub> (0.1M), 20 mL	0.25	6	7%	<5%
6	MeCN:DMSO(95:5)/Et <sub>4</sub> NBF <sub>4</sub> (0.1M), 20 mL	0.50	12	20%	12%

**Table 2:** Electrochemical synthesis of γ-lactones **2a** and **2b** by conjugate umpolung.<sup>a</sup>

<sup>a</sup>Divided cell, carbon-filled polyvinylidene fluoride (C/PVDF) anode, stainless steel cathode, alkaline pretreated Nafion® 438 membrane as compartments separator, room temperature, N<sub>2</sub> atmosphere, galvanostatic conditions (134 mA), catholyte: BMImBF<sub>4</sub>/MeCN 0.1 M, 20 mL (2 mmol BMImBF<sub>4</sub>); 1 mmol of cinnamaldehyde added at the end of the electrolysis to the catholyte. <sup>b</sup>With respect to the starting BMImBF<sub>4</sub>. <sup>c</sup>Isolated yields, based on starting cinnamaldehyde.

Table 2 reports the results obtained by changing the analyte composition and the amount of applied electricity. In all cases, with regards to the *trans/cis* diastereomeric ratio, we observed that the *cis* isomers **2a** were predominantly formed. The diastereoselectivity was not high; however, *trans* and *cis*  $\gamma$ -butyrolactones were easily

separated by column chromatography. Increasing the applied charge from 0.5 F (Table 2, entry 1) to 1.0 F (entry 2) improved the yield of both *cis* (**2a**) and *trans* (**2b**) lactones by approximately three fold. Instead, with a charge of 2.0 F the yield of **2a** improved by 10%, but the yield of **2b** increased only 2% (entry 3). However, in these experiments methyl ester **3a** was isolated as by-product derived from the methanol, which passed through the membrane, reacting with Breslow intermediate through a redox neutral process (Scheme 5) [19].



**Scheme 5.** Byproduct obtained from the reaction between methanol and Breslow intermediate.

We decided to use 1 F/mol and a lower amount of methanol at the anode, in order to minimise the formation of by-product **3a**; the same amount of **2a** was obtained, but the yield of *trans* diastereoisomer increased from 24% to 32% (Table 2, entry 2 *vs* entry 4). Finally, changing methanol with DMSO in the anolyte, a lower amount of both diastereoisomers was observed (entries 5 and 6). Thus the best yield (79%, 67/33 *cis/trans* ratio) was obtained using a charge of 2.0 F and a solution of MeCN:MeOH (9.5:0.5)/Et<sub>4</sub>NBF<sub>4</sub> (0.1 M) as anolyte (Table 2, entry 3).

#### Electrogenerated NHC organocatalysis. Esterification of trans

#### cinnamaldehyde

Once the possibility of obtaining the Breslow intermediate was demonstrated, another typical reaction of N-heterocyclic carbenes was tested: the oxidative esterification of cinnamaldehyde in the presence of alcohols. To carry out these experiments three different alcohols (methyl, isopropyl and benzyl alcohols) were used and the results are shown in Table 3.

All the experiments were carried out using a solution 0.1 M of BMImBF<sub>4</sub> in acetonitrile (20 mL) as catholyte, stainless steel as cathode, C/PVDF as anode, in a divided cell, under N<sub>2</sub> atmosphere, at room temperature, under galvanostatic conditions (I = 134 mA, t<sub>electrolysis</sub> = 12 min) with flow rate of 36 mL/min, anode solution as in Table, and

with 1.0 Faraday per mole of aldehyde. At the end of the electrolysis, 1 mmol of cinnamaldehyde was added to the catholyte and the mixture was left under stirring for five minutes and then the corresponding alcohol was added and the reaction was stirred for two hours at room temperature. Workup and column chromatography yielded esters **3a-c** and unsaturated esters **4a-c** as byproducts.

Table	3.	Electrochemical	synthesis	of	esters	3а-с	from	cinnamaldehyde	and	an
alcoho	l.a									

BI	$MIm^+ \frac{+e^-}{-0.5 H_2}$	► NHC			
NI	HC + Ph	$\begin{array}{c} O \\ H \\ \hline H$	ຊ <sup>3</sup> + Pr ອ າ r	$ \begin{array}{c} 0 \\ 4a \ R^{3} = M \\ 4b \ R^{3} = E \\ 4c \ R^{3} = 0 \end{array} $	DR <sup>3</sup> 1e 3n <i>i</i> Pr
Entry	ROH	Anolyte	Q (F) <sup>b</sup>	Via	
			- (- )	Tiel	a
1	R <sup>3</sup> =Me	MeCN:MeOH (98:2)/Et₄NBF₄ 0.1 M, 20 mL	0.5	<b>3a</b> 68%	<b>d</b> ° <b>4a</b> 11%
1	R <sup>3</sup> =Me R <sup>3</sup> =Bn	MeCN:MeOH (98:2)/Et <sub>4</sub> NBF <sub>4</sub> 0.1 M, 20 mL MeCN:BnOH (98:2)/Et <sub>4</sub> NBF <sub>4</sub> 0.1 M, 20 mL	0.5	3a 68% 3b 73%	<b>d</b> <sup>°</sup> 4a 11% 4b 13%

<sup>a</sup>Divided cell, carbon-filled polyvinylidene fluoride (C/PVDF) anode, stainless steel cathode, alkaline pretreated Nafion® 438 membrane separator, room temperature, N<sub>2</sub> atmosphere, galvanostatic conditions (134 mA), catholyte: BMImBF<sub>4</sub>/MeCN 0.1 M, 20 mL (2 mmol BMImBF<sub>4</sub>); 1 mmol of cinnamaldehyde added at the end of the electrolysis to the catholyte and, after 5 minutes 2 mmol of the corresponding alcohol were added. <sup>b</sup>With respect to the starting BMImBF<sub>4</sub>, t<sub>electrolysis</sub> = 12 min. <sup>c</sup>Isolated yields, based on starting cinnamaldehyde.

Good yields were obtained using benzyl and methyl alcohols (73% and 68% respectively), while with the isopropyl alcohol the formation of the ester was only

37%, probably due to steric hindrance. In two cases (Entries 1 and 2) oxidation byproducts (esters **4a** and **4b**) were obtained, where the olefinic double bond is preserved. In contrast to the internal redox reactions of cinnamaldehyde giving esters **3a–c**, formation of enoate by-products **4a** and **4b** invoke the involvement of an external chemical oxidant species as cinnamaldehyde is added to the cathode chamber after the electrolysis has been stopped. The presence of byproducts **4a** and **4b** is most likely accounted for by the presence of molecular oxygen, or electrochemically generated superoxide (cathodic reduction of O<sub>2</sub>), which oxidise the Breslow intermediate [30, 38]. In fact, presence of some reactive oxygen species in the reaction environment was previously demonstrated by the formation of the compound **1b** (see Table 1).

#### **IL Recycling**

To investigate the possibility to recycle BMImBF<sub>4</sub>, the experiment reported in Table 3, entry 1, was replicated, using the same reagents and conditions. Exploiting the low vapour pressure of BMImBF<sub>4</sub>, (and of ILs in general), the organic solvent was removed under reduced pressure, and after the extractive workup, the recycled BMImBF<sub>4</sub> was resubjected to cathodic reduction (thus reused in different reactions). Although this procedure led to decreased yields of esterification products **3a/4a** (10% and 12%, respectively) and diastereoisomeric 4-phenyl-5-styryldihydrofuran-2(3*H*)-ones **2a/b** (35%, 45:55 *cis/trans* mixture), the potential of the recycled BMImBF<sub>4</sub> to function as a N-heterocyclic carbene precursor was demonstrated. Interestingly, the reaction selectivity is completely lost using the recovered IL, and experiments are undergoing in order to understand the cause of this selectivity loss.

#### Batch vs Flow electrolysis

At this point, the preliminary results from flow electrochemistry may be compared with those reported in the literature for NHC formation using batch electrolysis. The comparison between these two techniques is not straightforward. In fact, in batch electrosynthesis, the ionic liquid is normally used as solvent, but in this work the IL was present as a 0.1 M solution in MeCN.

As regards the results obtained in the synthesis of thione **1a** (the only reaction for which a reasonable comparison is possible), we compared the current efficiencies,

the current being the limiting factor (Table 4). Although the current yield (49%) for the batch electrolysis in pure IL is higher than in flow, the yields for 0.1 M solutions are comparable between batch (29%) and flow (32%). In this case, the rate of production of the NHC in the electrolysis step was higher in the flow reactor (1.60 mmol/h) than in batch using pure IL (0.37 mmol/h). However, other factors should also be highlighted, including the 8x larger electrode area in the flow reactor, which enables a higher current to be passed while maintaining the same current density (15 mA/cm<sup>2</sup>). In the case of the NHC organocatalysis, we compared chemical yields of products (Table 4), although in different solvents. As far as the literature allows comparison of the flow electrochemistry conditions is required, it provides a valid alternative to batch technique. Again, productivity for the esterification is four-fold higher (3.65 mmol/h, 0.1 M solution) in flow than in batch (0.97 mmol/h, pure IL), and in flow the reaction volume could simply be increased to allow scale-up.

Product	Solvent	BATCH ELECTROCHEMISTRY Yield (current density)	FLOW ELECTROCHEMISTRY Yield (current density)
Me Ń S	BMImBF₄	49% <sup>a</sup> (15 mA/cm²)	-
N Bu 1a	Solvent/BMImBF <sub>4</sub>	29% <sup>b</sup> (15 mA/cm²)	32% <sup>c</sup> (15 mA/cm²)
Ph 2a-b Ph	MeCN/BMImBF4	-	79% <sup>d</sup> (15 mA/cm²)
	BMImBF <sub>4</sub>	91% <sup>e</sup> (20 mA/cm <sup>2</sup> )	-
3a	MeCN/BMImBF4	-	73% <sup>f</sup> (15 mA/cm²)

 Table 4: Comparison between electrosynthesis in batch and flow electrochemistry.

<sup>a</sup> Current yield. Q = 193 C. Theoretical current for a mono-electron process: 96.5 C for 1.0 mmol substrate/product. Current yield: (experimental yield/ theoretical yield) $\times$ 100. Ref. 37.

<sup>b</sup> Current yield (see note a). DMF as solvent. Ref. 12.

<sup>c</sup> Current yield (see note a). MeCN as solvent.

<sup>d</sup> Chemical yield, with respect to starting cinnamaldehyde. 2.0 F/mol cinnamaldehyde.

<sup>e</sup> Chemical yield, with respect to starting cinnamaldehyde. 0.7 F/mol cinnamaldehyde. 0.97 mmol/h. Ref. 39.

<sup>f</sup> Chemical yield, with respect to starting cinnamaldehyde. 3.65 mmol/h. 1.0 F/mol cinnamaldehyde.

## Conclusions

The results reported in this work demonstrate for the first time the possibility to synthesize and accumulate N-heterocyclic carbene starting from BMImBF<sub>4</sub> in a divided electrochemical flow cell. Although not fully optimized, the production of NHC was confirmed indirectly by isolation of its reaction product with elemental sulfur. A solution of the electrogenerated carbene was used to promote dimerization and oxidative esterification reactions of cinnamaldehyde. Under the flow conditions investigated, a higher rate of NHC production was achieved, compared to previously reported batch reactions, which is an important consideration for scale up. In the case of the flow procedure, a 0.1 M solution of the IL is employed, which may be more convenient than using pure IL. Further investigation of electrogeneration of NHCs and applications in organic synthesis are underway.

## Experimental

#### Materials and methods

Chemicals were purchased from Sigma–Aldrich and Alfa Aesar and used as received. All air/moisture sensitive reactions were carried out under an inert atmosphere, in oven-dried or flame-dried glassware. TLC was performed on aluminium plates precoated with silica gel 60 with an  $F_{254}$  indicator; visualized under UV light (254 nm) and/or by staining with potassium permanganate. Flash column

chromatography was performed using high purity silica gel, pore size 60 Å, 230–400 mesh particle size, purchased from Merck. <sup>1</sup>H NMR and <sup>13</sup>C NMR spectra were recorded in CDCl<sub>3</sub> (purchased from Cambridge Isotope Laboratories) at 298 K using Bruker DPX400 (400 and 101 MHz respectively) spectrometer. Chemical shifts are reported on the  $\delta$  scale in ppm and were referenced to residual solvent (CDCl<sub>3</sub>: 7.27 ppm for <sup>1</sup>H-NMR spectra and 77.0 ppm for <sup>13</sup>C-NMR spectra). Coupling constants (*J*) were given in Hz and matched where possible. The following abbreviations for the multiplicity of the peaks are used: s (singlet), d (doublet), t (triplet), q (quartet) and m (multiplet).

#### Parallel plate divided flow cell



**Figure 3**. Expanded view of the electrochemical cell components: (a) Aluminium end plates; (b) insulating PTFE foil, (c) copper plate for electrical contact; (d) carbon electrode; (e) PTFE gasket (reaction channel and sealing); (f) Nafion® membrane; (g) stainless steel electrode; (h) stainless-steel plate/electrode for electrical contact. Figure 3 was adapted from [36] with permission from The Royal Society of Chemistry. This content is not subject to CC BY 4.0.

The details about the dimensions of each cell component are reported elsewhere [36].

## General procedure for the synthesis of 1-butyl-3-methyl-1*H*imidazole-2(3*H*)-thione

Constant current electrolyses (I = 134 mA) were carried out using a parallel plate divided cell. Anolyte (25 mL) and catholyte (20 mL) were separated through a Nafion® 438 membrane. The anode material was carbon-filled polyvinylidenefluoride (C/PVDF) and the cathode material is described in Table 1. Electrolyses were carried out at room temperature, under nitrogen atmosphere, using a solution 0.1 M of BMImBF<sub>4</sub> in acetonitrile as catholyte. Anolyte solution is given in Table 1. Electrolyte solutions were continuously passed (recycling method) through their respective compartments at a flow rate of 36 mL/min. After consumption of the requisite amount of charge (Faradays per mol of BMImBF<sub>4</sub> reported in Table 1), the current was switched, the flow stopped, and elemental sulfur (2.0 mmol) was added to the catholyte. The mixture was left under ultrasound irradiation for 30 minutes. Solvent was removed under reduced pressure and the residue was purified by column

chromatography on silica gel (petroleum ether/ethyl acetate = 7/3), affording the corresponding pure **1a** as an off-white solid.

#### 1-Butyl-3-methyl-1*H*-imidazole-2(3*H*)-thione (1a)

Spectral data are consistent with those reported in the literature [37]. <sup>1</sup>H NMR (CDCl<sub>3</sub>)  $\delta$ : 6.64 (s, 2H), 3.99 (t, 2H, *J* = 7.4 Hz), 3.57 (s, 3H), 1.79-1.64 (m, 2H), 1.39-1.28 (m, 2H), 0.92 (t, 3H, *J* = 7.3 Hz) ppm. <sup>13</sup>C NMR (CDCl<sub>3</sub>)  $\delta$ : 162.3, 117.5, 116.4, 47.8, 35.0, 30.9, 19.7, 13.6 ppm.

#### 1-Butyl-3-methyl-1*H*-imidazol-2(3*H*)-one (1b)

Spectral data are consistent with those reported in the literature [39]. <sup>1</sup>H NMR (CDCl<sub>3</sub>)  $\delta$ : 6.19 (d, AB,  $\Delta v/J = 2.5$ ,  $\Delta v = 7.1$  Hz, J = 2.8 Hz, 1H), 6.17 (d, AB,  $\Delta v/J = 2.5$ ,  $\Delta v = 7.1$  Hz, J = 2.8 Hz, 1H), 3.59 (t, 2H, J = 7.2 Hz), 3.24 (s, 3H), 1.70-1.59 (m, 2H), 1.42-1.24 (m, 2H), 0.92 (t, 3H, J = 7.2 Hz) ppm. <sup>13</sup>C NMR (CDCl<sub>3</sub>)  $\delta$ : 153.1, 111.3, 110.2, 43.5, 31.1, 30.5, 19.9, 13.6 ppm.

#### General procedure for dimerization of trans cinnamaldehyde

Constant current electrolyses (I = 134 mA) were carried out using a parallel plate divided cell. Anolyte (20 mL) and catholyte (20 mL) were separated through a Nafion® 438 membrane. The anode material was carbon-filled polyvinylidenefluoride C/PVDF and stainless steel for the cathode material. Electrolyses were carried out at room temperature, under nitrogen atmosphere, using a solution 0.1 M of BMImBF<sub>4</sub> in acetonitrile as catholyte and for anolyte solution see table 2, which were passed (recycling method) in their compartments with a flow rate of 36 mL/min. After the consumption of the number of Faradays per mol of BMImBF<sub>4</sub> reported in Table 2, the current was switched off, the flow stopped and cinnamaldehyde (1.0 mmol) was added to the catholyte. The mixture was stirred for 2 h. Solvent was removed under reduced pressure and the residue was extracted with of Et<sub>2</sub>O (15 mL x 3) and then purified by column chromatography on silica gel (petroleum ether/ethyl acetate = 9/1), affording the corresponding pure products **2a** and **2b**.

(±) cis 4-Phenyl-5-((E)-styryl)dihydrofuran-2(3H)-one (2a)

Spectral data are consistent with those reported in the literature [40]. <sup>1</sup>H NMR (CDCl<sub>3</sub>)  $\delta$ : 7.38-7.25 (m, 3H), 7.29-7.24 (m, 3H), 7.23-7.15 (m, 4H), 6.63 (d, 1H, *J* = 15.9 Hz), 5.65 (dd, 1H, *J* = 15.9 Hz, 6.5 Hz), 5.42-5.38 (m, 1H), 3.99-3.93 (m, 1H), 2.98 (dd, 1H, *J* = 17.4 Hz, 8.1 Hz), 2.91 (dd, 1H, *J* = 17.4 Hz, 7.4 Hz) ppm. <sup>13</sup>C NMR (CDCl<sub>3</sub>)  $\delta$ : 176.3, 136.9, 135.8, 133.4, 128.9, 128.6, 128.2, 127.9, 127.8, 126.6, 123.8, 83.5, 45.6, 34.3 ppm.

#### (±) trans 4-Phenyl-5-((E)-styryl)dihydrofuran-2(3H)-one (2b)

Spectral data are consistent with those reported in the literature [40]. <sup>1</sup>H NMR (CDCl<sub>3</sub>)  $\delta$ : 7.39-7.27 (m, 10H), 6.60 (d, 1H, *J* = 15.9 Hz), 6.23 (dd, 1H, *J* = 15.9 Hz, 6.7 Hz), 5.06-5.02 (m, 1H), 3.57-3.50 (m, 1H), 3.04 (dd, 1H, *J* = 17.5 Hz, 8.6 Hz), 2.87 (dd, 1H, *J* = 17.5 Hz, 10.5 Hz) ppm. <sup>13</sup>C NMR (CDCl<sub>3</sub>)  $\delta$ : 175.2, 138.0, 135.6, 133.8, 129.2, 128.7, 128.4, 127.9, 127.3, 126.8, 124.7, 86.7, 48.4, 36.7 ppm.

#### General procedure for the esterification of *trans* cinnamaldehyde

Constant current electrolyses (I = 134 mA) were carried out using a parallel plates divided cell. Anolyte (20 mL) and catholyte (20 mL) were separated through a Nafion® 438 membrane. The anode material was C/PVDF and stainless steel for the cathode material. Electrolyses were carried out at room temperature, under nitrogen atmosphere, using a solution 0.1 M of BMImBF<sub>4</sub> in acetonitrile as catholyte. Anolyte solution is given in Table 3. Electrolyte solutions were continuously passed (recycling method) through their respective compartments at a flow rate of 36 mL/min. After the consumption of 0.5 F/mol of BMImBF<sub>4</sub> (12 min, 96 C), the current was switched off, the flow stopped and cinnamaldehyde (1.0 mmol) was added to the catholyte. The mixture was left under stirring for 5 minutes and then the corresponding alcohol (2.0 mmol) was removed under reduced pressure and the residue was extracted with of Et<sub>2</sub>O (15 mL x 3) and purified by column chromatography on silica gel (petroleum ether/ethyl acetate = 9.5/0.5), affording the corresponding pure esters **3a-c** and **4a-b**.

#### **BMImBF**<sub>4</sub> Recycling procedure

After extraction of product **3a** from the solution, the catholyte was placed under vacuum at room temperature for 30 min to remove diethyl ether residues, then it was

used as catholyte for a new electrolysis (see section 3.4 to repeat the same procedure).

#### Methyl 3-phenylpropanoate (3a)

Spectral data are consistent with those reported in the literature [41]. <sup>1</sup>H NMR (CDCl<sub>3</sub>)  $\delta$ : 7.32–7.23 (m, 2H), 7.22–7.14 (m, 3H), 3.65 (s, 3H), 2.94 (t, 2H, *J* = 7.9 Hz), 2.62 (dd, 2H, *J* = 8.4 Hz, 7.3 Hz) ppm. <sup>13</sup>C NMR (CDCl<sub>3</sub>)  $\delta$ : 173.3, 140.5, 128.5, 128.5, 128.5, 128.3, 126.3, 51.6, 35.7, 30.9 ppm.

#### Benzyl 3-phenylpropanoate (3b)

Spectral data are consistent with those reported in the literature [42]. <sup>1</sup>H NMR (CDCl<sub>3</sub>)  $\delta$ : 7.19-7.39 (m, 10H), 5.13 (s, 2H), 2.99 (t, 2H, *J* = 7.0 Hz), 2.70 (t, 2H, *J* = 7.0 Hz) ppm. <sup>13</sup>C NMR (CDCl<sub>3</sub>)  $\delta$ : 172.7, 140.4, 136.0, 128.6, 128.5, 128.3, 128.2, 126.3, 66.3, 35.9, 31.0 ppm.

#### Isopropyl 3-phenylpropanoate (3c)

Spectral data are consistent with those reported in the literature [43]. <sup>1</sup>H NMR (CDCl<sub>3</sub>)  $\delta$ : 7.28-7.36 (m, 2 H), 7.19-7.27 (m, 3 H), 4.99-5.11 (m, 1 H), 2.99 (t, J = 7.5 Hz, 2 H), 1.24 (d, 6 H, *J* = 6.3 Hz) ppm. <sup>13</sup>C NMR (75 MHz, CDCl<sub>3</sub>)  $\delta$ : 172.5, 140.6, 128.5, 128.4, 126.2, 67.8, 36.3, 31.1, 21.8 ppm.

#### Methyl cinnamate (4a)

Spectral data are consistent with those reported in the literature [44]. <sup>1</sup>H NMR (CDCl<sub>3</sub>)  $\delta$ : 7.69 (d, 1H, *J* = 16.0 Hz), 7.58–7.45 (m, 2H), 7.41 – 7.32 (m, 3H), 6.43 (d, 1H, *J* = 16.0 Hz), 3.78 (s, 3H) ppm. <sup>13</sup>C NMR (CDCl<sub>3</sub>)  $\delta$  167.4, 144.8, 134.4, 130.3, 128.9, 128.1, 117.8, 51.7 ppm.

#### Benzyl cinnamate (4b)

Spectral data are consistent with those reported in the literature [45]. <sup>1</sup>H NMR (CDCl<sub>3</sub>)  $\delta$ : 7.73 (d, 1H, *J* = 16.0 Hz), 7.56–7.49 (m, 2H), 7.45–7.31 (m, 8H), 6.49 (d, 1H, *J* = 16.0 Hz), 5.26 (s, 2H) ppm. <sup>13</sup>C NMR (CDCl<sub>3</sub>)  $\delta$  166.8, 145.2, 136.1, 136.0, 134.3, 130.4, 128.9, 128.6, 128.29, 128.26, 128.1, 117.9, 66.4 ppm.

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